

Case study

Hydraulic calculations & irrigation schedule

Pump selection

1 - IRRIGATION SCHEDULE

SHIFT	CONTROLLERS					CON. FLOW	CONTROLLERS					CON. FLOW	TOTAL GPM	RUN TIME	TOTAL GPD
	CONTROL-1						CONTROL-2								
1	B1	B2	B3	B4		128.00	B19	B20	B21			110.00	238.00	15.00	3,570.00
	25.00	32.00	32.00	39.00			39.00	39.00	32.00						
2	B5	B6	B7			124.00	B22	B24	B25			107.00	231.00	15.00	3,465.00
	35.00	39.00	50.00				39.00	36.00	32.00						
3	B8	B9	B10	B11	B12	121.00	B26	B27	B28	B29	B30	118.00	239.00	15.00	3,585.00
	39.00	15.00	14.00	25.00	28.00		18.00	21.00	8.00	39.00	32.00				
4	B13	B14	B15	B16		180.00	B31	B32				64.00	244.00	15.00	3,660.00
	35.00	57.00	35.00	53.00			32.00	32.00							
5	B17	B18	B23	B35	B36	128.00	B33	B34				68.00	196.00	15.00	2,940.00
	35.00	39.00	18.00	18.00	18.00		32.00	36.00							
8	D1	D2	D3	D4	D5	128.40	D19	D20	D21	D22		118.10	246.50	30.00	7,395.00
	20.50	25.70	25.70	30.80	25.70		30.80	30.80	25.70	30.80					
9	D6	D7	D8	D9	D10	128.40	D24	D25	D26	D27	D28	102.70	231.10	30.00	6,933.00
	30.80	41.10	30.80	15.40	10.30		30.80	25.70	15.40	20.50	10.30				
10	D11	D12	D13	D14	D15	138.60	D29	D30	D31			90.20	228.80	30.00	6,864.00
	20.50	20.50	25.70	46.20	25.70		38.80	25.70	25.70						
11	D16	D17	D18	D23	D35	128.40	D32	D33	D34			89.80	218.20	30.00	6,546.00
	41.10	25.70	30.80	15.40	15.40		25.70	36.00	28.10						
												MINUTES	195.00	44,958.00	GPD
												HAUR	03:15	170.17	M3/D
NOTES:															
1.Total irrigation time per cycle is 3:15 hours.															
2.Total consumption of water per irrigation cycle is 171 cubic meters.															
3. Run time indicated for plants at maturity.At every stage of plant needs adjustment.															

- The head loss calculations based on shift no. 11 as it is the widest shift and contain 2 of furthest valves (D34 & D33)

② - friction loss calculations

- The equations used in calculations as follow:-

- **darcy-weisbach equation (pipes)** $H_f = f \left(\frac{L}{D} \right) \frac{v^2}{2g}$ where:-

- H_f = friction head (loss) in pipe

- L = pipe length

- D = pipe inner diameter

- v = flow velocity

- g = gravitational acceleration = 9.81 m/s²

- f = friction factor, calculated from **swamee-jain equation**

- **swamee-jain equation** $f = \frac{0.25}{\left[\log_{10} \left(\frac{\epsilon}{3.7D} + \frac{5.74}{Re^{0.9}} \right) \right]^2}$ where:-

- ϵ = pipe surface Roughness

- **Re** = *renold number* = $Re = \frac{v * D}{\text{kinematic viscosity}}$

- **flow velocity** = $V = \frac{Q}{A}$ where:-

- **Q** = flow rate

- **A** = pipe inner cross sectional area

- *darcy-weisbach equation (fittings)* $H_f = K \frac{v^2}{2g}$ where:-

- **K** = friction factor for each fitting given from Cameron hydraulic handbook or any reference, and illustrated below in the calculation sheets.

- **Valve flow coefficient** $K_v = Q(m^3/h) \sqrt{\frac{SG}{\Delta p(bar)}}$ where SG=water specific gravity = 1

- **total dynamic head = TDH** = friction head (H_f) + static head (H_s)

3 - auxiliary data taken in calculation

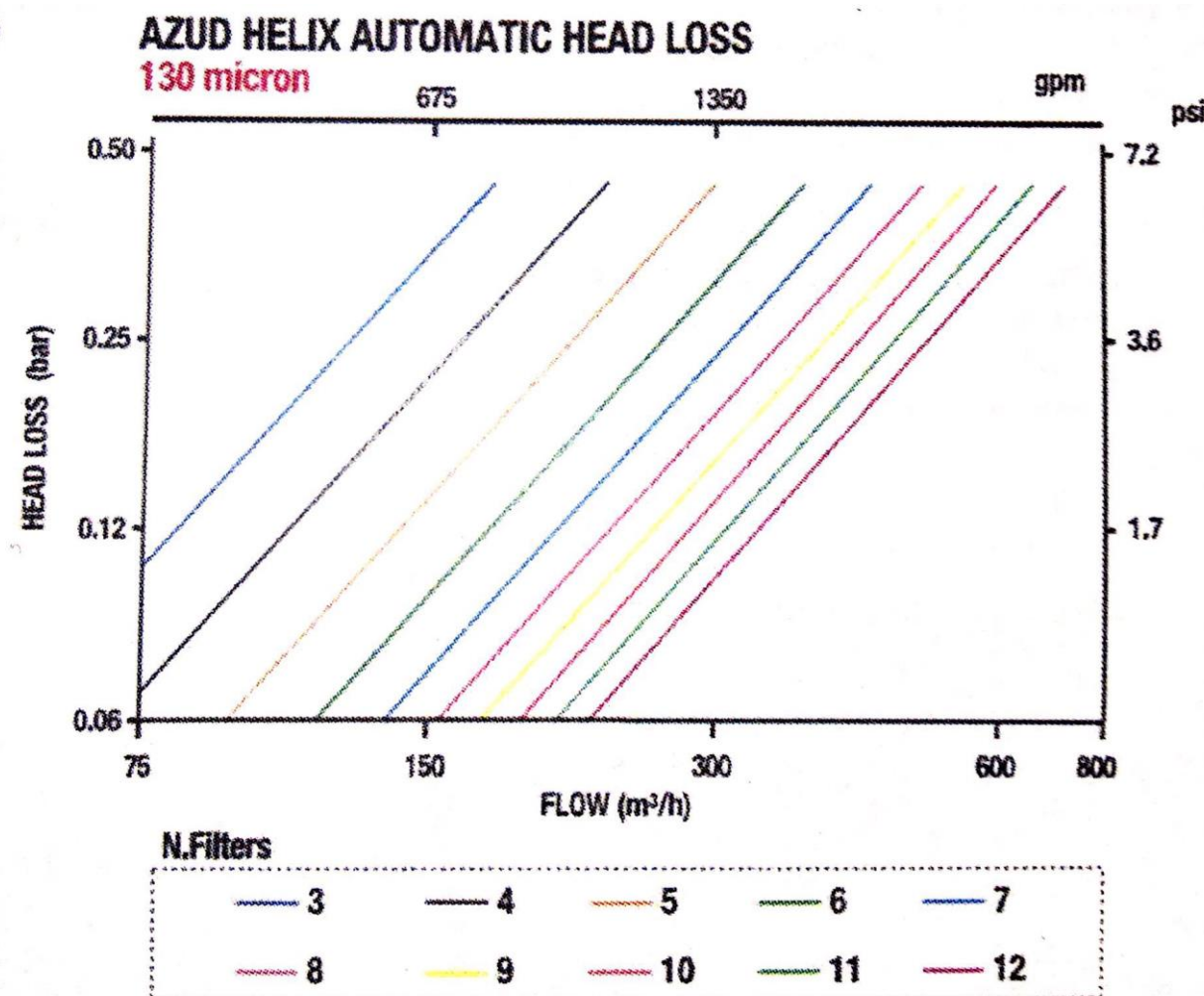
According the studied network the below data is required in calculation as follow:-

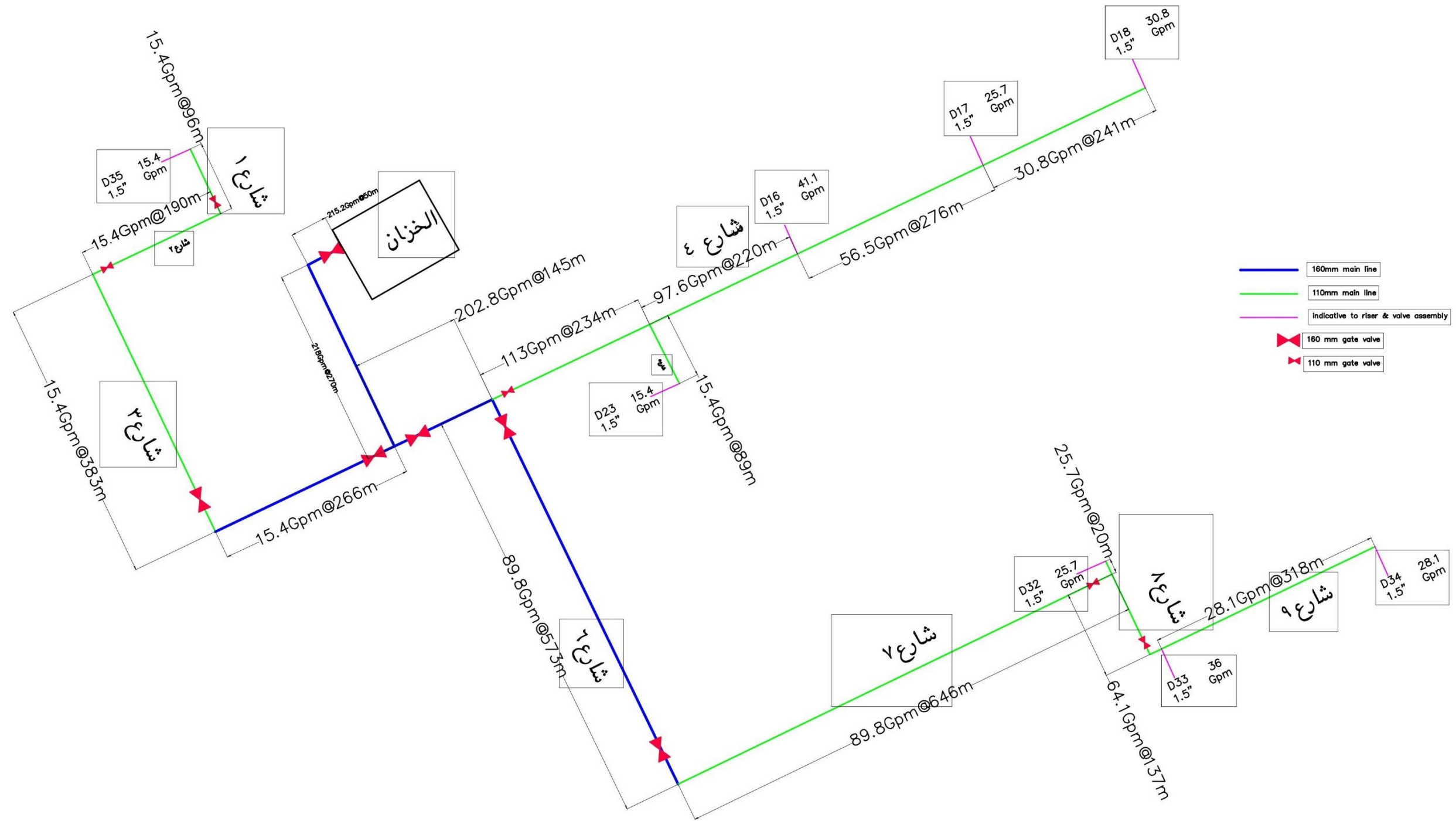
- Pvc pipe 160mm class5 inner diameter= $D=136.2$ mm
- Pvc pipe160mm class5 inner cross sectional area = $A=0.014569482$ m²
- Pvc pipe 110mm class5 inner diameter= $D=93.6$ mm
- Pvc pipe110 class5 inner cross sectional area= $A=0.006880842$ m²
- Pvc pipe 63mm class5 inner diameter= $D=53.6$ mm
- Pvc pipe 63 class5 inner cross sectional area = $A=0.002256418$ m²
- Pvc pipe 50mm class5 inner diameter= $D=42.6$ mm
- Pvc pipe 50mm class5 inner cross sectional area = $A=0.001425309$ m²
- Pvc pipe 32mm class5 inner diameter= $D=27.2$ mm

- Pvc pipe 32mm class5 inner cross sectional area = $A = 0.000581069 \text{ m}^2$
- Pvc pipe 20mm class5 inner diameter = $D = 17 \text{ mm}$
- Pvc pipe 20mm class5 inner cross sectional area = $A = 0.00022698 \text{ m}^2$
- Pvc pipes surface roughness = $\epsilon = 0.0015 \text{ mm}$
- Steel pipe 6 inch inner diameter = $D = 154.08 \text{ mm}$
- Steel pipe 6 inch inner cross sectional area = $A = 0.01864586 \text{ m}^2$
- Steel pipes surface roughness = $\epsilon = 0.046 \text{ mm}$
- Ductile pipe 6 inch inner diameter = $D = 159.258 \text{ mm}$
- Ductile pipe 6 inch cross sectional area = $A = 0.01992014 \text{ m}^2$
- Ductile pipe surface roughness = $\epsilon = 0.5 \text{ mm}$
- Water kinematic viscosity = $1 \text{ Cst} = 1 \text{ mm}^2/\text{s} = 10^{-6} \text{ m}^2/\text{s}$
- K factors for each fitting illustrated in the calculation sheet
- Static head = the difference in level between tank water level and highest valve
= $HS = 7 \text{ m}$

4 - the studied network geometry and dimensions

- The below drawing illustrate the studied network(irrigation network only without pump room)
- Pump room components calculations illustrated directly in calculations sheets considering its actual geometry and dimensions
- Friction loss across the Disc filter in the pump room taken from the below curve (given from supplier or manufacturer)



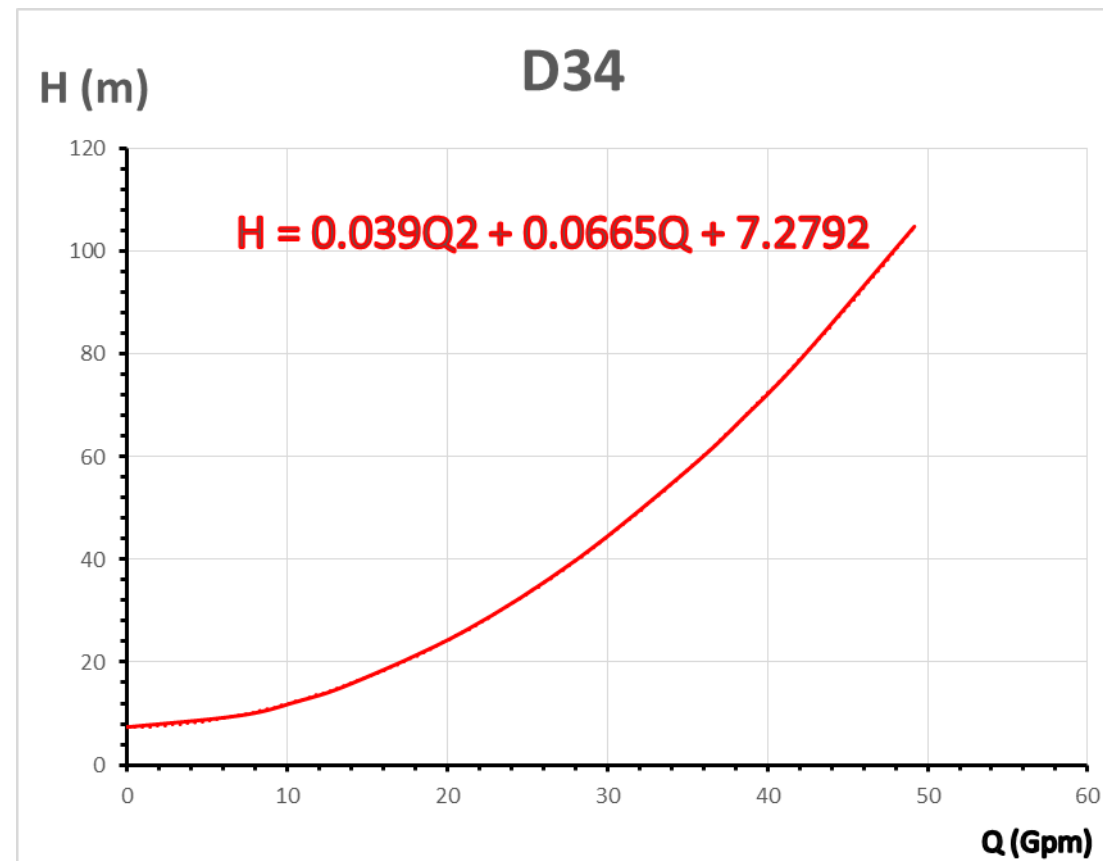


main lines network dimensions

5 - main lines friction loss calculations

- Calculation based on the above mentioned network geometry and dimensions
- The above illustrated drawing dimensions may slightly differ while construction
- The pump room geometry and dimensions was not illustrated in the above drawing but taken directly within the calculations sheets
- The main line friction loss calculations made after lateral line calculations, and take the values of lateral lines total dynamic head while main calculations
- The later line calculations are illustrated by the end of this calculation note in section 17
- These calculation based on assumed static head **Hs = 7m** (the difference in level between water level and valve level)
- The calculations made for each valve in **shift no.11** individually
- The calculations based on a range of flow rates including the intended flow rate of the intended valve to construct system curve keeping the same ratios of flow rates range while calculate each valve
- Pumps characteristic curves were picked up from **KSB** data sheets

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
7.025	0.870395	7	1.274645	9.602293
10.5375	1.803294	7	2.867952	12.25481
14.05	3.033555	7	5.098581	15.88874
21.075	6.341575	7	11.47181	26.05405
28.1	10.73179	7	20.39432	40.03242
35.125	16.16502	7	31.86613	57.78271
38.6375	19.26375	7	38.55802	68.06286
42.15	22.66889	7	45.88723	79.33393
49.175	30.46551	7	62.45762	104.9193



Q(G pm)	TDH (m)
0	7.35
7.543326	10
17.22785	20
23.29928	30
28.12539	40
32.25532	50
35.92436	60
39.25919	70
42.33728	80
45.21014	90
47.91406	100
50.47573	110

- **D34** is full open and its friction drop calculated directly = $\Delta p = Hf = K \frac{v^2}{2g}$ where K is friction factor for globe valve full open = 7.1
- **D34** require no calculations of Kv

Step1- Δp of (D33@36GPM)=TDH(D34@28.1GPM)-TDH(D33)=1.35974 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D33) is the total dynamic head of D33 path before calculating Hf of D33 solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m^3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv = 22

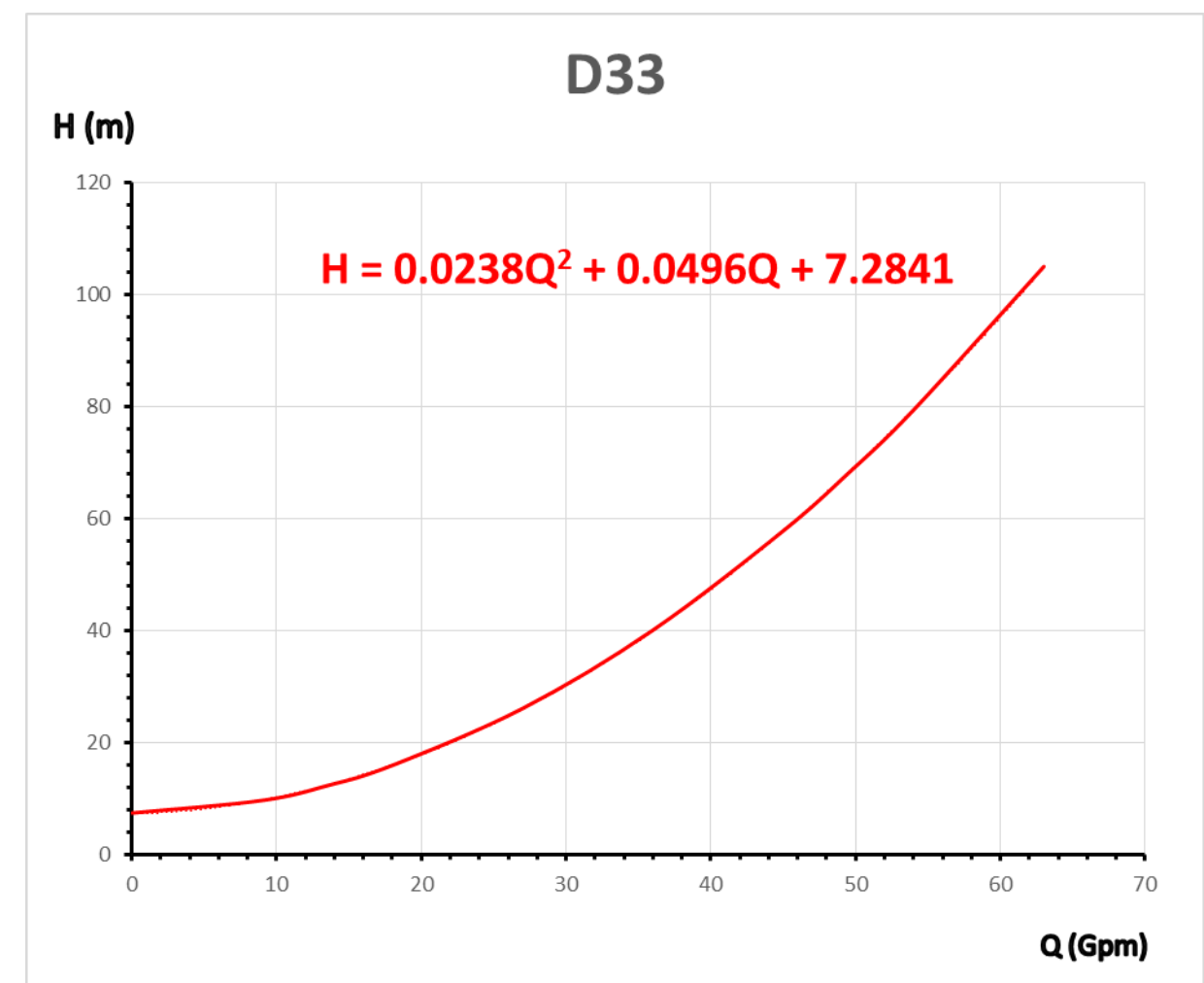
step3- $\Delta p = \frac{Q^2}{Kv^2}$

solenoid valve calculations			
Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
9	2.044122	0.084984	0.008334
13.5	3.066184	0.191214	0.018752
18	4.088245	0.339935	0.033336
27	6.132367	0.764854	0.075007
36	8.176489	1.35974	0.133345
45	10.22061	2.124594	0.208352
49.5	11.24267	2.570759	0.252105
54	12.26473	3.059416	0.300026
63	14.30886	4.164205	0.408369

Step4

Q(G pm)	Hf	Hs	lateral line	TDH
0	0	7	0	7.35
9	0.862651	7	1.274645	9.594162
13.5	1.792033	7	2.867952	12.24298
18	3.020241	7	5.098581	15.87476
27	6.330113	7	11.47181	26.04202
36	10.7318	7	20.39432	40.03243
45	16.18747	7	31.86613	57.80629
49.5	19.30186	7	38.55802	68.10287
54	22.72575	7	45.88723	79.39363
63	30.56947	7	62.45762	105.0284

Step5



Step6

Q(G pm)	TDH
0	7.35
9.691074	10
22.09599	20
29.86972	30
36.04846	40
41.33571	50
46.03281	60
50.302	70
54.24248	80
57.92021	90
61.38163	100
64.66095	110

Step1- Δp of (D32@25.7GPM)=TDH(D34@28.1GPM)-TDH(D32)=2.277778 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D33) is the total dynamic head of D32 path before calculating Hf of D32 solenoid valve, then it recalculated and corrected again after Calculating Kv

Step2- $Kv = Q(m^3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
Kv=12.35

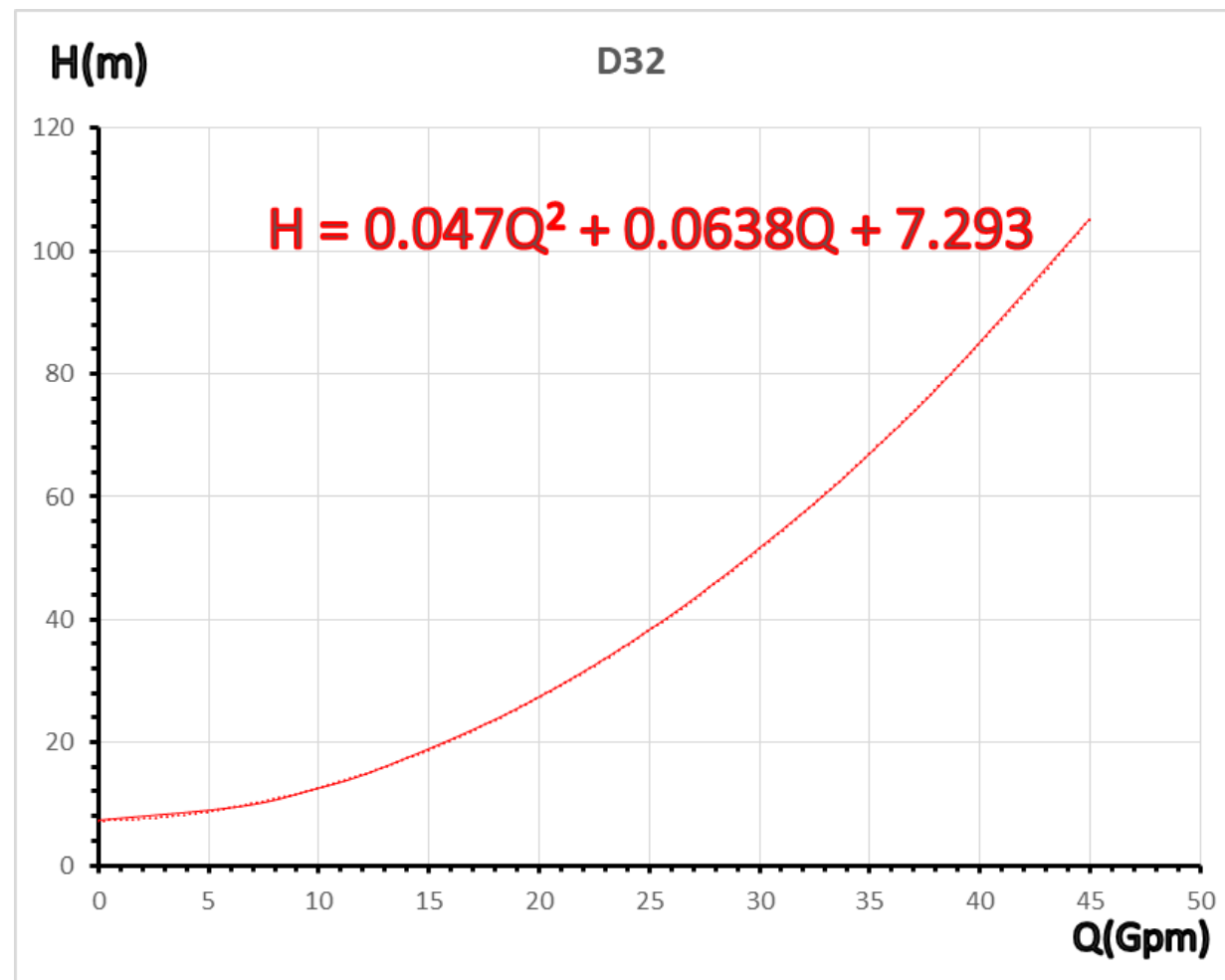
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
6.425	1.459276	0.142361	0.013961
9.6375	2.188914	0.320313	0.031412
12.85	2.918552	0.569445	0.055843
19.275	4.377829	1.281251	0.125648
25.7	5.837105	2.277778	0.223374
32.125	7.296381	3.55903	0.349022
35.3375	8.026019	4.306426	0.422316
38.55	8.755657	5.125003	0.502591
44.975	10.21493	6.975698	0.684082

Step4

Q(Gpm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
6.425	0.849786	7	1.274645	9.580653
9.6375	1.773135	7	2.867952	12.22314
12.85	2.997756	7	5.098581	15.85115
19.275	6.3106	7	11.47181	26.02153
25.7	10.73179	7	20.39432	40.03242
32.125	16.22598	7	31.86613	57.84672
35.3375	19.36732	7	38.55802	68.17161
38.55	22.82353	7	45.88723	79.4963
44.975	30.74863	7	62.45762	105.2166

Step5



Step6

Q(G pm)	TDH (m)
0	7.35
6.940752	10
15.77796	20
21.31192	30
25.7098	40
29.4729	50
32.81585	60
35.85417	70
38.65851	80
41.27582	90
43.73918	100
46.07292	110

Step1- Δp of (D18@30.8GPM)=TDH(D34@28.1GPM)-TDH(D18@30.8GPM)
 =1.916787302 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D18) is the total dynamic head of **D18** path before calculating **Hf** of **D18** solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m^3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv=16.14

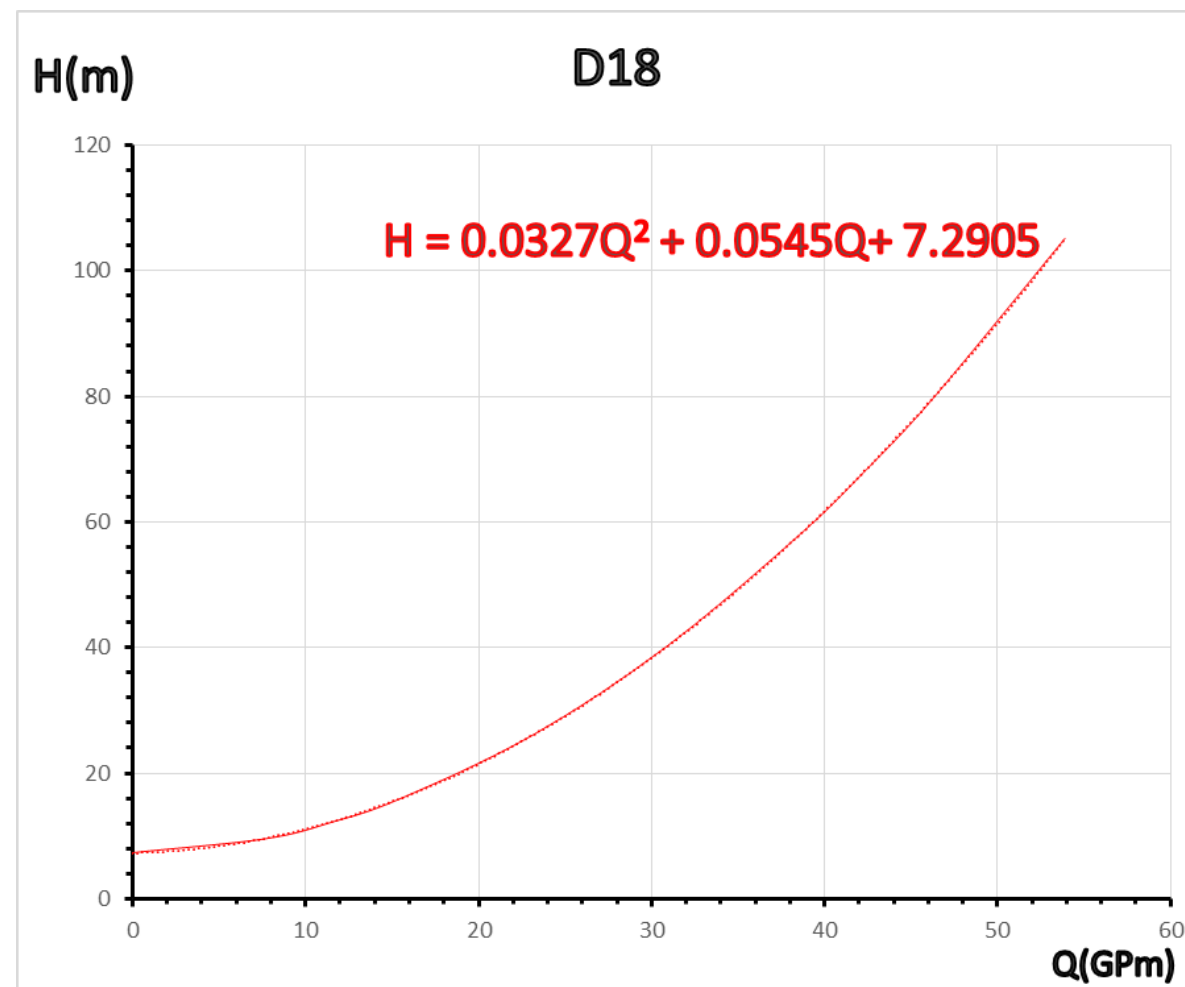
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
7.7	1.74886	0.119799	0.011748
11.55	2.62329	0.269547	0.026434
15.4	3.49772	0.479194	0.046993
23.1	5.246581	1.078187	0.105734
30.8	6.995441	1.916787	0.187973
38.5	8.744301	2.994964	0.293706
42.35	9.618731	3.623906	0.355384
46.2	10.49316	4.312748	0.422936
53.9	12.24202	5.870129	0.575663

Step4

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
7.7	0.853374	7	1.274645	9.58442
11.55	1.778418	7	2.867952	12.22869
15.4	3.004049	7	5.098581	15.85776
23.1	6.316058	7	11.47181	26.02726
30.8	10.73179	7	20.39432	40.03242
38.5	16.2152	7	31.86613	57.8354
42.35	19.34902	7	38.55802	68.15239
46.2	22.79622	7	45.88723	79.46763
53.9	30.6987	7	62.45762	105.1641

Step5



Step6

Q(G pm)	TDH (m)
0	7.35
8.307442	10
18.89898	20
25.53283	30
30.80501	40
35.31629	50
39.32393	60
42.96639	70
46.32837	80
49.46614	90
52.41934	100
55.21716	110

Step1- Δp of (D17@25.7GPM)=TDH(D34@28.1GPM)-TDH(D17@30.8GPM)
 =2.34249 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D17) is the total dynamic head of **D17** path before calculating **Hf** of **D17** solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m^3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv=12.18

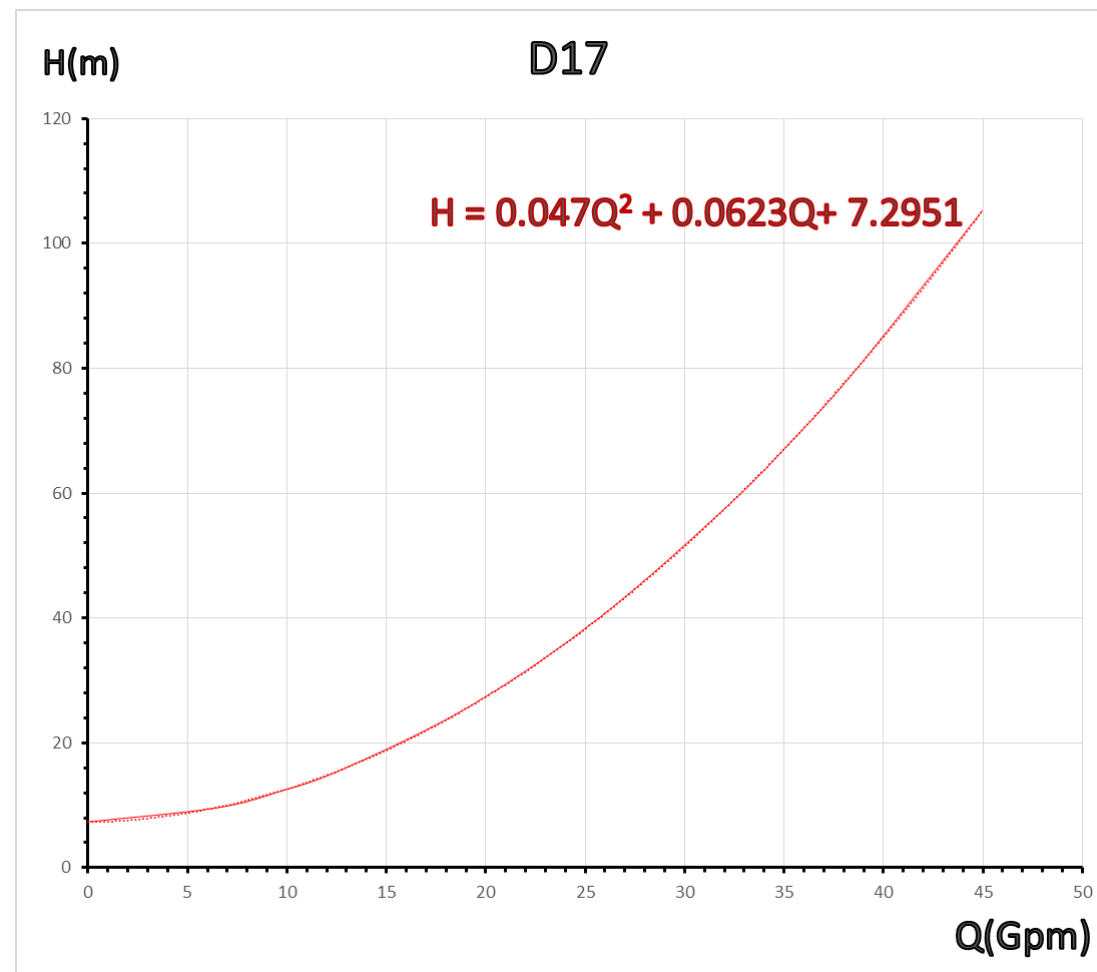
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
6.425	1.459276	0.146406	0.014358
9.6375	2.188914	0.329414	0.032304
12.85	2.918552	0.585625	0.05743
19.275	4.377829	1.317656	0.129218
25.7	5.837105	2.342487	0.229719
32.125	7.296381	3.660156	0.358939
35.3375	8.026019	4.428789	0.434316
38.55	8.755657	5.270625	0.516872
44.975	10.21493	7.173906	0.70352

Step4

Step5

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
6.425	0.846226	7	1.274645	9.576915
9.6375	1.768007	7	2.867952	12.21776
12.85	2.991727	7	5.098581	15.84482
19.275	6.305442	7	11.47181	26.01611
25.7	10.73179	7	20.39432	40.03242
32.125	16.23608	7	31.86613	57.85732
35.3375	19.38445	7	38.55802	68.18959
38.55	22.84908	7	45.88723	79.52313
44.975	30.79536	7	62.45762	105.2656



Step6

Q(G pm)	TDH (m)
0	7.35
6.952372	10
15.79191	20
21.32637	30
25.72451	40
29.48776	50
32.83082	60
35.86922	70
38.67363	80
41.29099	90
43.75439	100
46.08817	110

Step1- Δp of (D16@41.1GPM)=TDH(D34@28.1GPM)-TDH(D16@41.1GPM)
 =2.57137 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D16) is the total dynamic head of **D16** path before calculating **Hf** of **D16** solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv=18.6

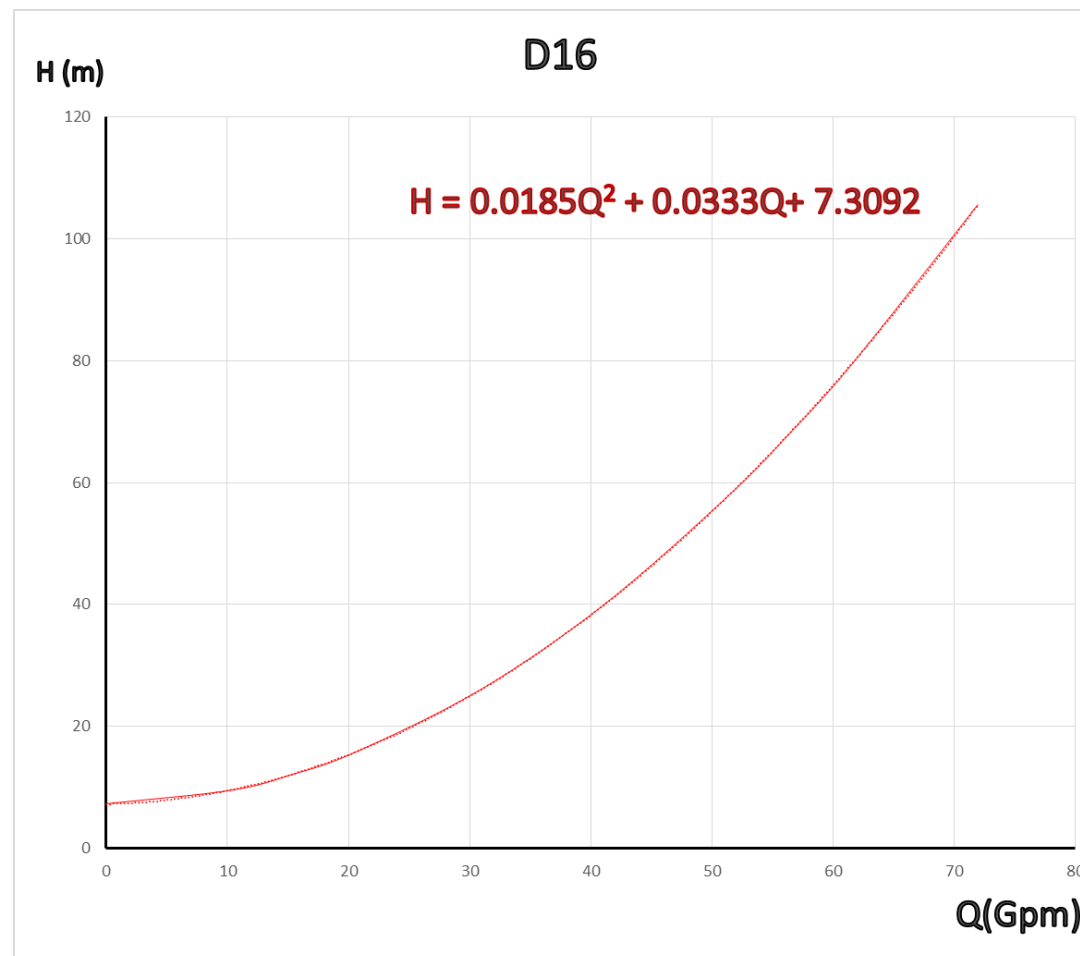
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
10.275	2.333706	0.160711	0.01576
15.4125	3.50056	0.3616	0.035461
20.55	4.667413	0.642844	0.063041
30.825	7.001119	1.446399	0.141843
41.1	9.334825	2.571374	0.252166
51.375	11.66853	4.017776	0.394009
56.5125	12.83539	4.861509	0.476751
61.65	14.00224	5.785597	0.567373
71.925	16.33594	7.87484	0.772258

Step4

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
10.275	0.825392	7	1.274645	9.555039
15.4125	1.737459	7	2.867952	12.18568
20.55	2.955421	7	5.098581	15.8067
30.825	6.273977	7	11.47181	25.98307
41.1	10.73179	7	20.39432	40.03242
51.375	16.29808	7	31.86613	57.92242
56.5125	19.48981	7	38.55802	68.30022
61.65	23.00645	7	45.88723	79.68836
71.925	31.08361	7	62.45762	105.5683

Step5



Step6

Q(G pm)	TDH (m)
0	7.35
11.19374	10
25.30685	20
34.13341	30
41.14617	40
47.14603	50
52.47566	60
57.31943	70
61.79005	80
65.96242	90
69.88929	100
73.60949	110

12 - valve D23 calculations

	Range of flow rates								
	Q1	Q2	Q3	Q4	Q5	Q6	Q7	Q8	Q9
D35	3.85	5.775	7.7	11.55	15.4	19.25	21.175	23.1	26.95
D23	3.85	5.775	7.7	11.55	15.4	19.25	21.175	23.1	26.95
D16	10.275	15.4125	20.55	30.825	41.1	51.375	56.5125	61.65	71.925
D17	6.425	9.6375	12.85	19.275	25.7	32.125	35.3375	38.55	44.975
D18	7.7	11.55	15.4	23.1	30.8	38.5	42.35	46.2	53.9
D32	6.425	9.6375	12.85	19.275	25.7	32.125	35.3375	38.55	44.975
D33	9	13.5	18	27	36	45	49.5	54	63
D34	7.025	10.5375	14.05	21.075	28.1	35.125	38.6375	42.15	49.175

flow velocity

$$V = \frac{Q}{A}$$

Reynold number

$$Re = \frac{v * D}{kinematic\ viscosity}$$

swamee-jain equation

$$f = \frac{0.25}{[\log_{10}(\frac{\epsilon}{3.7D} + \frac{5.74}{Re^{0.9}})]^2}$$

darcy-weisbach equation (pipes)

$$Hf = f \left(\frac{L}{D}\right) \frac{v^2}{2g}$$

darcy-weisbach equation (fittings)

$$Hf = K \frac{v^2}{2g}$$

D23 path elements	Q(Gpm)									V(m/s)									Re									f									Hf (m H ₂ O)								
	Q1	Q2	Q3	Q4	Q5	Q6	Q7	Q8	Q9	V1	V2	V3	V4	V5	V6	V7	V8	V9	Re1	Re2	Re3	Re4	Re5	Re6	Re7	Re8	Re9	f1	f2	f3	f4	f5	f6	f7	f8	f9	Hf1	Hf2	Hf3	Hf4	Hf5	Hf6	Hf7	Hf8	Hf9
1- ductile pipe (L=1.7m & D=6")	54.55	81.825	109.1	163.65	218.2	272.75	300.025	327.3	381.85	0.172769	0.259154	0.345538	0.518307	0.691076	0.863845	0.95023	1.036614	1.209383	27514.85356	41272.28	55029.71	82544.56	11059.4	137574.3	151331.7	165089.1	192604	0.030883	0.029671	0.029006	0.028285	0.027898	0.027655	0.027563	0.027486	0.027363	0.000501541	0.011084	0.001884	0.004134	0.007249	0.011228	0.013541	0.016069	0.021774

Step1- Δp of (D23@15.4GPM)=TDH(D34@28.1GPM)-TDH(D23@15.4GPM)
 =5.20171 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D23) is the total dynamic head of D23 path before calculating Hf of D23 solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m^3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv=4.9

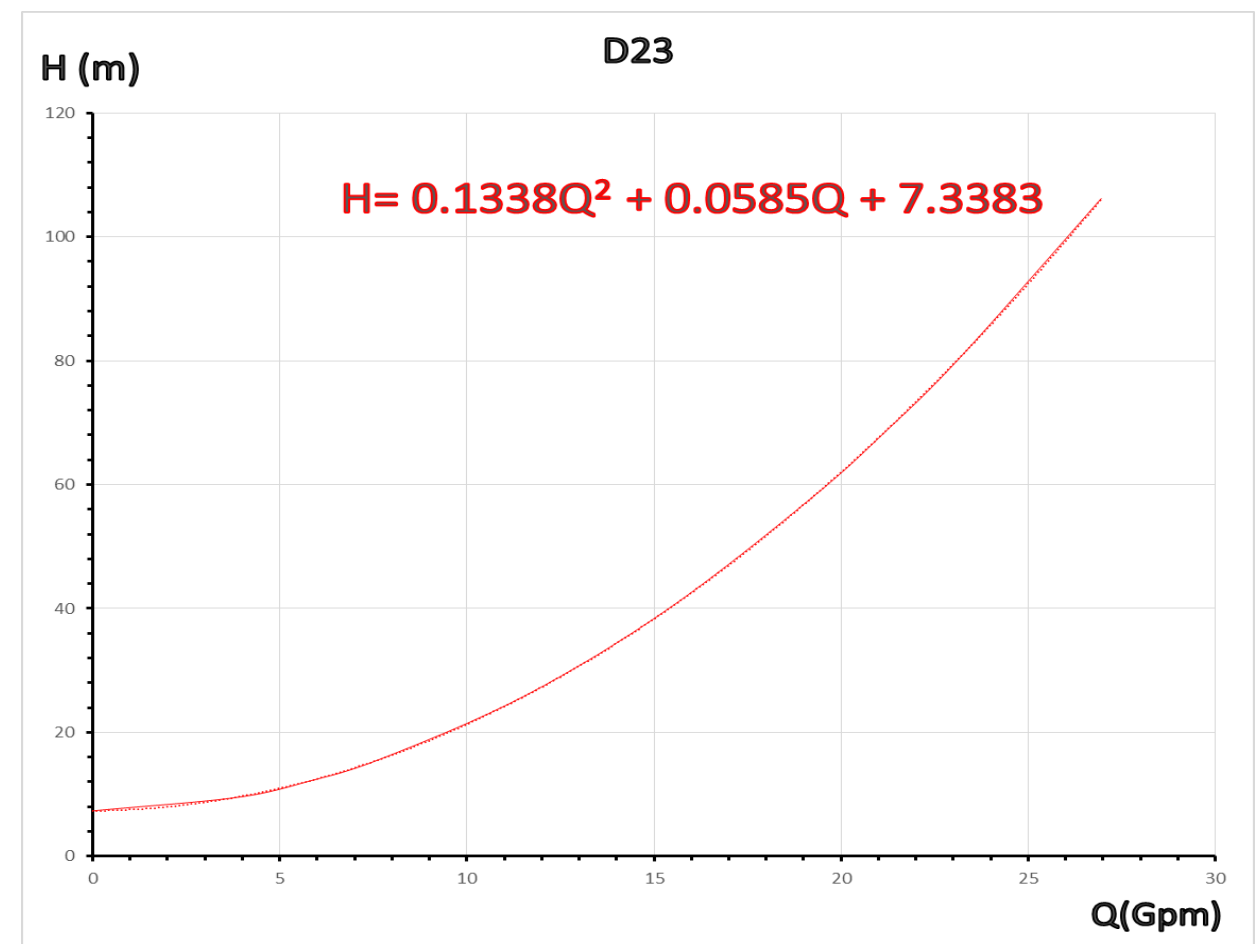
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
3.85	0.87443	0.325107	0.031882
5.775	1.311645	0.731492	0.071735
7.7	1.74886	1.300429	0.127529
11.55	2.62329	2.925966	0.286939
15.4	3.49772	5.201712	0.510114
19.25	4.372151	8.127683	0.797053
21.175	4.809366	9.834497	0.964435
23.1	5.246581	11.70386	1.147757
26.95	6.121011	15.93026	1.562225

Step4

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
3.85	0.783995	7	1.274645	9.511572
5.775	1.676425	7	2.867952	12.1216
7.7	2.882636	7	5.098581	15.73028
11.55	6.21064	7	11.47181	25.91657
15.4	10.73179	7	20.39432	40.03242
19.25	16.42347	7	31.86613	58.05408
21.175	19.70304	7	38.55802	68.52411
23.1	23.32508	7	45.88723	80.02292
26.95	31.66777	7	62.45762	106.1817

Step5



Step6

Q(G pm)	TDH (m)
0	7.35
4.246915	10
9.511721	20
12.79745	30
15.40689	40
17.63901	50
19.62158	60
21.42328	70
23.08611	80
24.63794	90
26.09843	100
27.48202	110

Step1- Δp of (D35@15.4GPM)=TDH(D34@28.1GPM)-TDH(D35@15.4GPM)
 =8.30424 m

$$\Delta p = \frac{Q^2}{Kv^2}$$

Note:- TDH(D35) is the total dynamic head of D35 path before calculating Hf of D35 solenoid valve, then it recalculated and corrected again after

Calculating Kv

Step2- $Kv = Q(m3/h) \sqrt{\frac{1}{\Delta p(bar)}}$
 Kv = 3.9

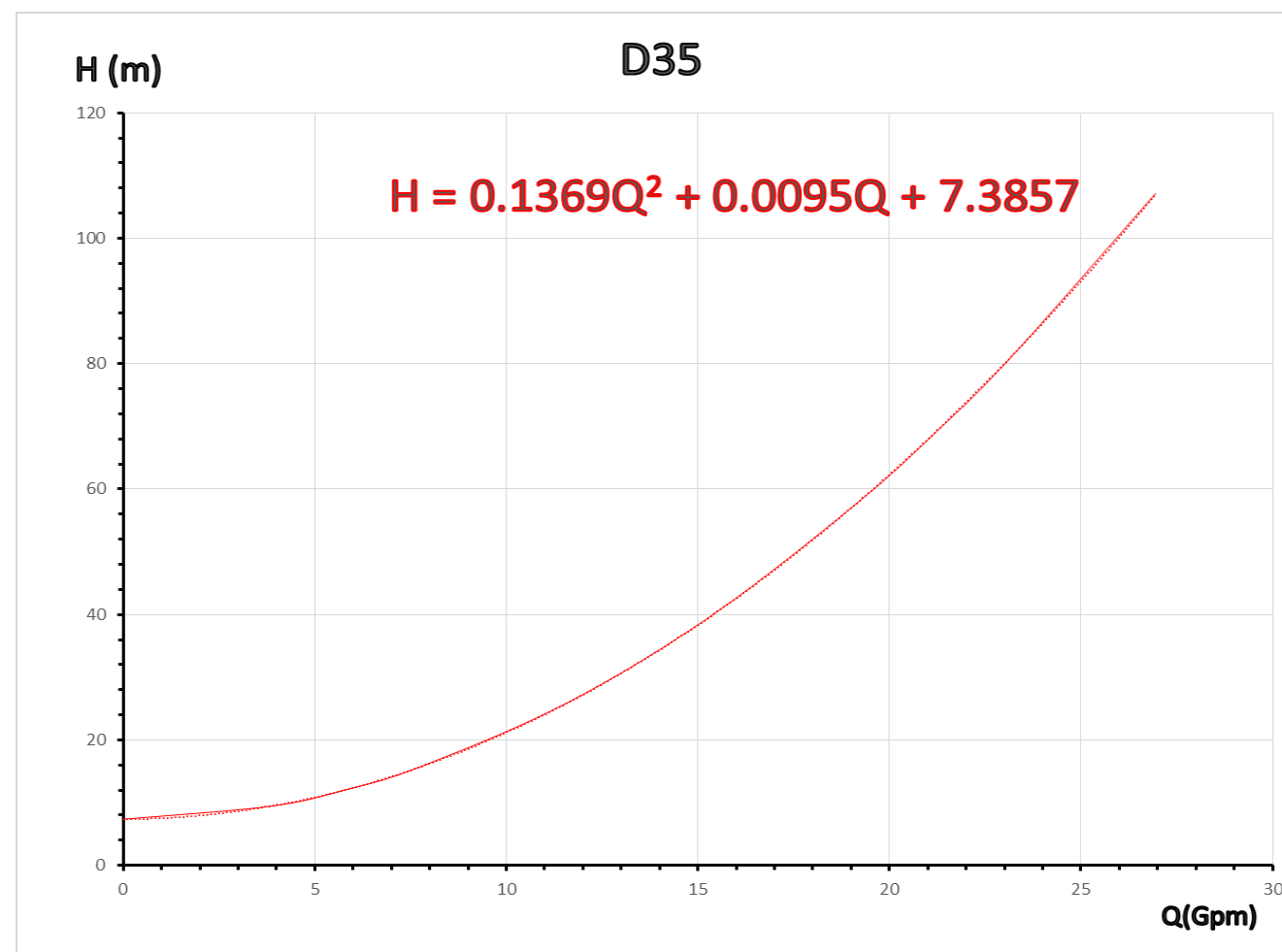
step3- $\Delta p = \frac{Q^2}{Kv^2}$

Q		Δp	
Gpm	m3/h	m	bar
0	0	0	0
3.85	0.87443	0.519015	0.050898
5.775	1.311645	1.167784	0.11452
7.7	1.74886	2.07606	0.203592
11.55	2.62329	4.671135	0.458082
15.4	3.49772	8.304243	0.814368
19.25	4.372151	12.97538	1.27245
21.175	4.809366	15.7002	1.539664
23.1	5.246581	18.68454	1.832328
26.95	6.121011	25.43174	2.494001

Step4

Q(G pm)	Hf	Hs	lateral line	TDH (m)
0	0	7	0	7.35
3.85	0.718263	7	1.274645	9.442554
5.775	1.579178	7	2.867952	12.01949
7.7	2.766417	7	5.098581	15.60825
11.55	6.109236	7	11.47181	25.8101
15.4	10.73179	7	20.39432	40.03242
19.25	16.62474	7	31.86613	58.26541
21.175	20.04546	7	38.55802	68.88366
23.1	23.83698	7	45.88723	80.56042
26.95	32.6069	7	62.45762	107.1677

Step5

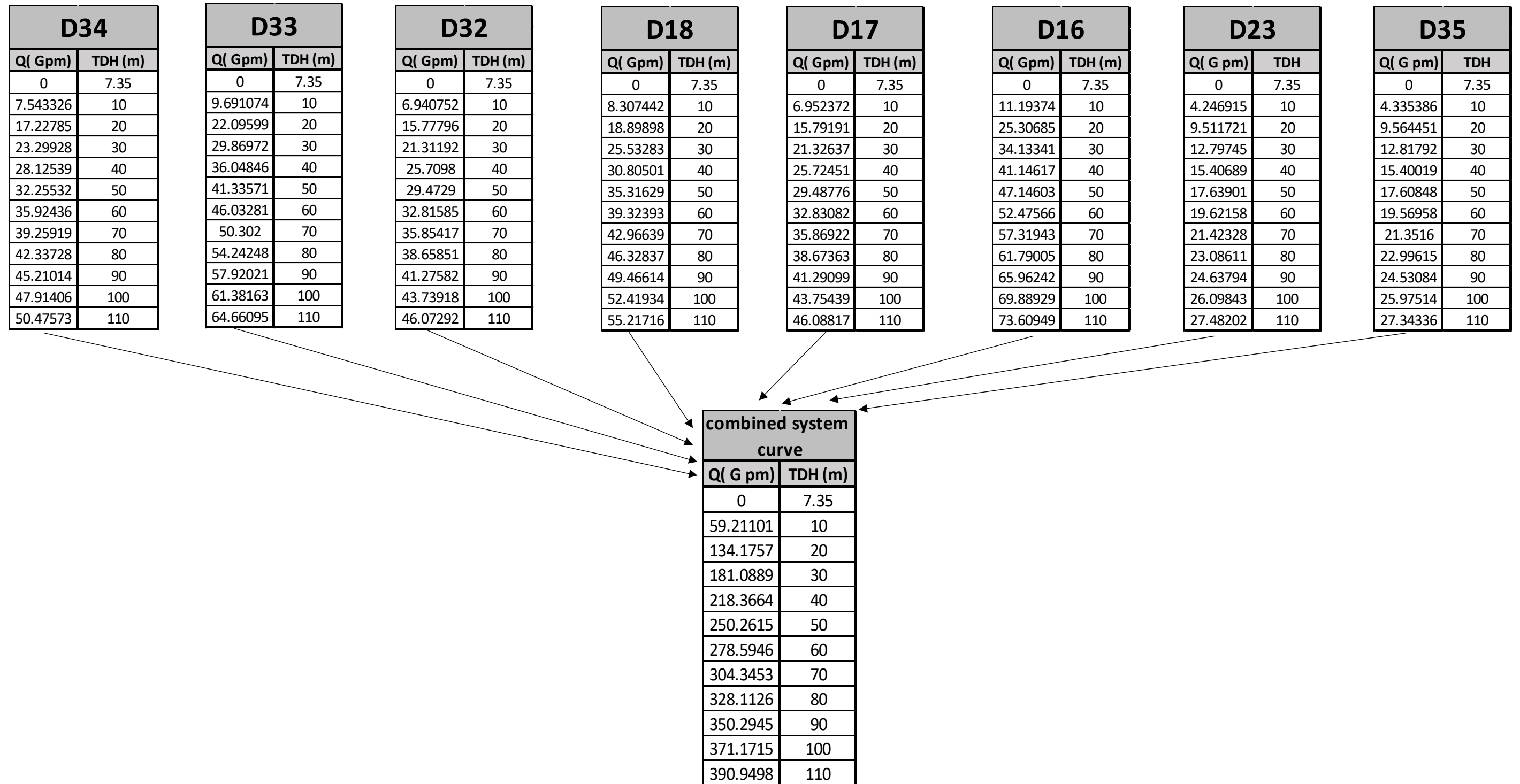


Step6

Q(G pm)	TDH (m)
0	7.35
4.335386	10
9.564451	20
12.81792	30
15.40019	40
17.60848	50
19.56958	60
21.3516	70
22.99615	80
24.53084	90
25.97514	100
27.34336	110

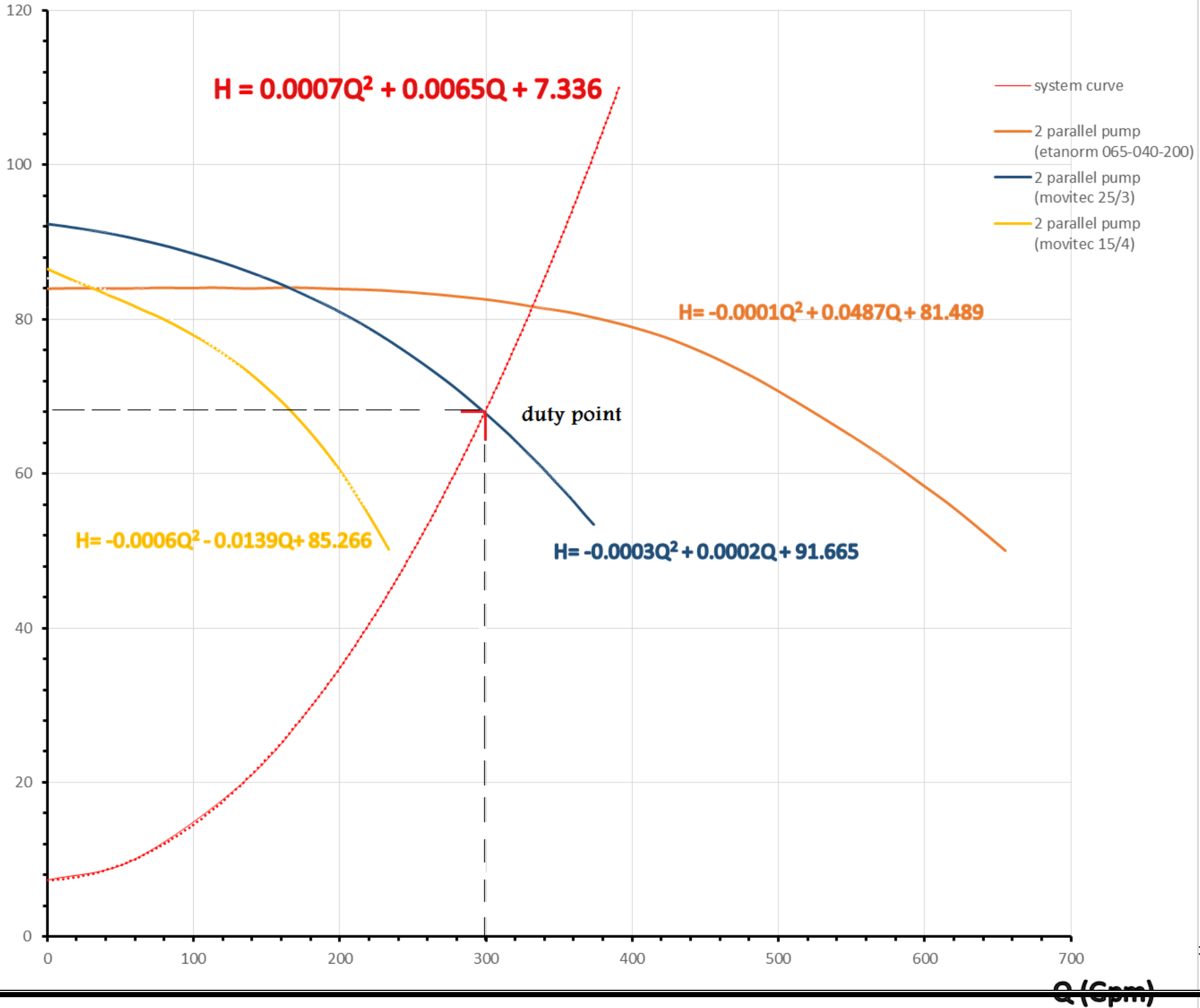
14 - system curve construction

- System curve constructed from the summation of (Q's) of individual valves at constant (H's) as follow



H (m)

combined system curve with pumps curves



15 - recommendations (selected pump)

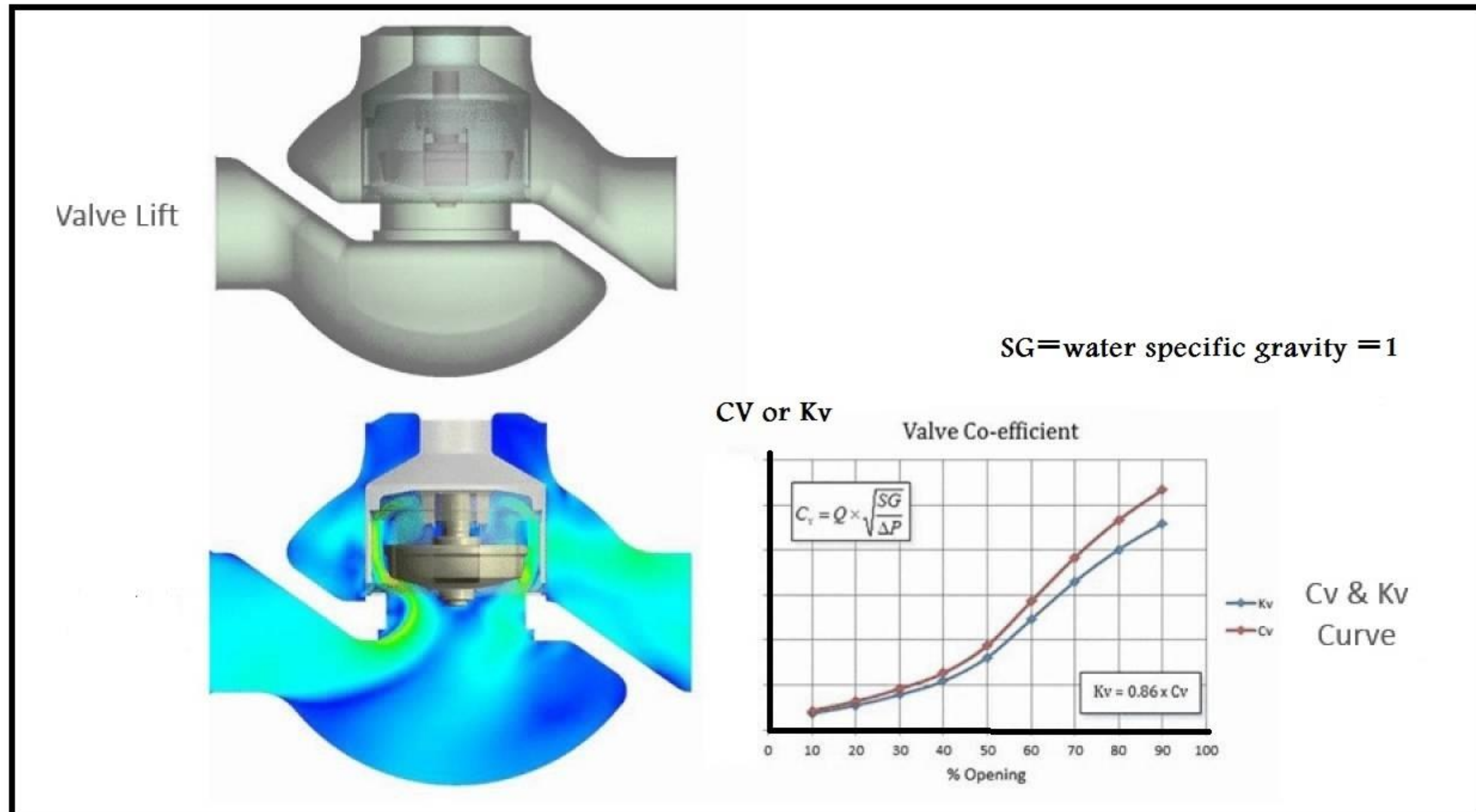
- After construct the system curve shown above and combine it with pumps curves for three different sets of pumps we recommend the set of ([2 parallel pumps KSB brand model movitec 25/3](#)) its nominal capacity according contractor BOQ (vertical centrifugal pump **Q=125 Gpm & H=5.5 bar**)
- Actual duty point of the 2 parallel pump set(**Q= 293Gpm & H=6.5 bar**)
- We recommend after construction of irrigation network, installation of pump room, testing, and commissioning to measure the actual flow as built at each irrigation shift, and recalculate run time of valves in irrigation schedule(decreasing or increasing) to meet you exact demands accurately

16 - valves adjusting

- According the upper calculation we recommend solenoid valve of flow control option to achieve network balancing and keep you exact demands, and adjust the valves flow control (valve opening) according the pre-calculated **Kv's** as follow

valve	valve Kv	valve opening
D33	22	
D32	12.3	
D18	16	
D17	12.2	
D16	18.6	
D23	4.9	
D35	3.9	

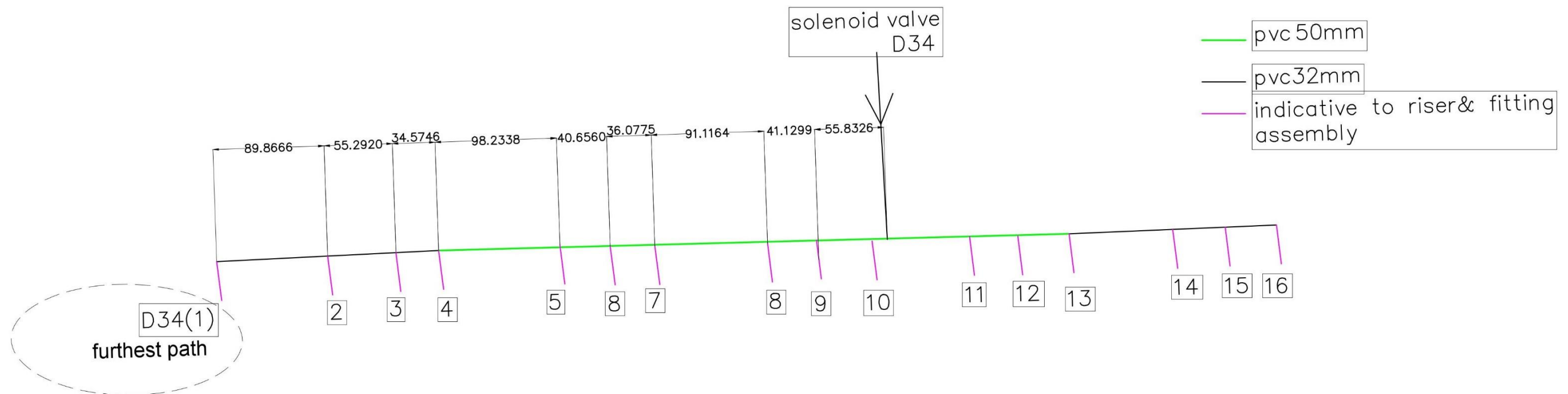
- Notice:- the actual valve opening according the above calculated **Kv's** is not defined here in this calculations you can get it from the valve manufacturer catalogues as follow:-
- (the below chart, just indicative but, it is not the actual for this design)



Notice:- this is indicative characteristic valve chart not the actual for you valves, just for illustration only

17 - later line calculations

- Lateral line calculation based on the the exit of solenoid valve **D34** the results of this lateral network calculations taken with safety factor to calculate the main calculations for all the valves of shift no-11 assuming they has approximately similar later network



lateral lines network dimensions

Q(Gpm)	Hf	Hst	exit pressure	TDH (m)
0	0	1	10	11
0.55	0.111948	1	10	11.11195
0.825	0.227469	1	10	11.22747
1.1	0.378083	1	10	11.37808
1.65	0.778769	1	10	11.77877
2.2	1.305886	1	10	12.30589
2.75	1.954408	1	10	12.95441
3.025	2.323047	1	10	13.32305
3.3	2.720776	1	10	13.72078
3.85	3.602276	1	10	14.60228

- From the above lateral calculation the **TDH** for the furthest path = 1.2 bar take it =2 bar in the main calculation of **D34 @ 28.1Gpm** and for **D34** range of flow rates keep the opposed lateral TDH using the relation between $H \propto Q^2$ or

$$\frac{H_1}{H_2} = \frac{Q_1^2}{Q_2^2}$$